

# **Herbal Extract Decolourization Device Using Activated Carbon**

Teh Liam Chee<sup>a\*</sup>, Rozilawati Abdul Gaffar, <sup>b</sup> Fadzilah Adibah Abdul Majid<sup>b</sup>, Mohammad Roji Sarmidi<sup>b</sup>

### Article history

Received :10 September 2012 Received in revised form :27 December 2012

Accepted:12 February 2013

### Graphical abstract



### Abstract

Herbal extracts are known for their antioxidant, antimicrobial, and anti-inflammatory properties. However, the intense colour caused by their phenolic content and dark-coloured compounds may spoil the final product's appearance. To remedy that, this study was undertaken to design a decolourization device to eliminate the intense colour of herbal extracts while retaining their beneficial properties. Batch experiments have been conducted to study decolourization and its effect on extract quality. From there, a decolourization device has been devised using activated carbon. Operating at optimum conditions, the device was able reduce 81 % of the total phenolic content of cashew leaf extracts while retaining 88 % of its radical scavenging capacity. Furthermore, the device is able to re-design the extract's colour to fulfill the end-user's needs by manipulating the contact period. The design of this device best fits Langmuir isotherm which demonstrates monolayer coverage of adsorbate at the outer surface of activated carbon.

Keywords: Activated carbon; adsorption; herbal extract; Langmuir Isotherm; decolourization

#### Abstrak

Ekstrak herba telah dikenali untuk kosmeseutikal dan sifat nutraseutikalnya seperti antioksidan, antimikrob, anti radang dan lain-lain. Walau bagaimanapun, warna yang pekat mungkin merosakkan penampilan produk disebabkan kandungan fenolik dan komponen warna gelap yang lain. Penyelidikan ini bertujuan untuk merekacipta satu alat pelunturan warna untuk menghilangkan warna pekat ekstrak tumbuhan sambil mengekalkan sifat berfaedah dengan menggunakan karbon teraktif. Eksperimen Batch telah dijalankan untuk mengkaji pelunturan warna dan prestasi kualiti ekstrak. Keadaan operasi yang optimum untuk 100 mL extrak daun gajus adalah menggunakan 5g serbuk karbon teraktif dan 5g butiran karbon teraktif, pada suhu 25°C dan 10 minit masa sentuhan. Keadaan ini menurunkan 81 % jumlah kandungan fenol dan mengekalkan 88% RSC estrak daun gajus. Reka bentuk sistem ini paling sesuai diterangkan dengan Langmuir isoterma yang menunjukkan liputan monolayer komponen fenolik dan warna gelap pada permukaan luar karbon teraktif. Kajian ini adalah percubaan pertama untuk menunjukkan potensi menggunakan karbon teraktif untuk melunturkan warna ekstrak herba. Satu kelebihan rekabentuk alat ini adalah bahawa pelunturan warna ekstrak herba boleh diubahsuai berdasarkan keperluan pengguna akhir dengan memanipulasi masa sentuhan.

Kata kunci: Karbon teraktif; adsorption; ekstrak herba; Langmuir Isoterma; pelunturan warna

© 2012 Penerbit UTM Press. All rights reserved.

# ■1.0 INTRODUCTION

Consumers nowadays are keen to ask for more effective and more natural products to maintain the wellbeing of their skin. As a result, more attention has shifted to cosmeceutical products with high antioxidant properties; Properties that could slow down the process of aging and rejuvenate skin. A source of safe, natural antioxidants is food plants that are rich in phenolic compounds.

One of the challenges of developing a cosmetic formulation from plants is the intense colour of the extracts that

may spoil the product's appearance. Phenolic compounds are the main contributor to the intense dark colour of the herbal extracts, making them unsuitable as an ingredient for cosmeceutical products even though they contain antioxidants and other beneficial properties. Hence, there is the pressing need to develop a procedure to eliminate the intense colour of herbal extracts while retaining their high antioxidant properties. The removal of polyphenolic compounds and their intense colour from herbal extracts using conventional methods is quite difficult without compromising the quality of the final product. For example, the use of chemicals as a bleaching agent to

<sup>&</sup>lt;sup>a</sup>Department of Bioprocess Engineering, Faculty of Chemical Engineering, Universiti Teknologi Malaysia, 81310 UTM Johor Bahru, Johor, Malaysia

<sup>&</sup>lt;sup>b</sup>Institute of Bioproduct Development (IBD), Universiti Teknologi Malaysia, 81310 UTM Johor Bahru, Johor, Malaysia

<sup>\*</sup>Corresponding author: lcteh86@gmail.com

remove the extracts' colour is not welcomed by consumers. Alternatively, some sort of adsorption process could be employed to remove phenolic and other coloured compounds from herbal extracts. Indeed, such a method is commonly used to purify contaminated fluids that smells and tastes bad. For such a task, a number of decolourizing agents are currently being used in the fruit juice industry to remove phenolic compound. Such decolourizing agents include activated carbon (AC), gelatine or bentonite, casein, ion-exchange resins and polyvinylpolypyrrolidone (PVPP) [1].

AC is widely used as a natural and cost effective adsorbent of colours and organic substances. This is due to its outstanding adsorptive ability and its wide variety of forms to suit different processing conditions. For this reason, the capacity of AC to remove phenolic and coloured compounds in food stuff and fruit juices as well as its application in waste water treatment have been extensively studied[1-6]. That being said, decolourization of herbal extracts using AC has yet been studied. For that, an AC separator system was designed and tested in this study to facilitate decolourization of herbal extracts. Of the various AC's physical forms, AC in the form of powder and granular are the most commonly used. Several parameters may influence the performance of AC as an adsorbent. The adsorptive characteristics of AC are mainly affected by its porous structure, surface area and its surface's chemical structure [7]. Other factors such the amount of AC used, operation temperature, and contact period of the samples with AC also play a role. These parameters have been investigated in this study to optimize the conditions required for optimum decolourization of herbal extracts using the AC separator system.

Cashew leaf extracts' antimicrobial activity and antityrosinase activity can be exploited for preserving and whitening purposes respectively, and hence is a potential cosmeceutical ingredient [8], [9]. Indeed, the cashew tree is a food plant known to possess quite a few medicinal properties. The shoots of cashew are freshly eaten as 'ulam' by the Malay community especially from the east coast of peninsular Malaysia for its rejuvenating effects. Aside from that, different parts of the plant have been widely used traditionally for sore gums and toothaches, sore throats, burns and skin diseases [10], [11]. Furthermore, cashew is also used to effectively remedy diarrhea and colic. On top of that, it is considered to be gentle enough to be taken by children [11]. Besides that, it was also reported that cashew leaf extracts have antiulcerogenic effect [10]. More importantly, it was recently demonstrated that cashew leaf extracts possess strong antioxidant activities [7], thus making it well suited to be a new active ingredient in cosmetic formulation with multiple functions.

Desirable characteristics that must be kept in mind in developing the decolourization device include simplicity of operation, ease of decolourization, affordability and availability of absorption materials, and the ability to be operated at room temperature with the absence of chemicals. The core component of the decolourization device consist of two layers; the upper layer that consists of powdered activated carbon with higher surface area, and the base layer that consists of granular activated carbon that prevents leaching of the powdered activated carbon above. Since the absorbability of granular and powdered activated carbon are different, it is important to investigate the ratio of these two forms of activated carbons with respect to the decolourization performance of the device on the extract.

This study was the first attempt to decolourize herbal extracts with AC and investigate the effects of the ratio between the two different forms of AC (powder and granular) on decolourization. The purpose of this study was to design and

optimize operating conditions for a device that decolourizes herbal extracts by AC adsorption. To this end, it was necessary to determine: (i) the optimum composition of two AC (granular and powder form) used, (ii) the respective effects of temperature and contact period on total polyphenolic content removal and antioxidant retention, and (iii) the best adsorption model (Langmuir, Freundlich, Frumkin or Temkin) to estimate AC adsorption capacity and isotherm parameters.

### ■2.0 MATERIAL AND METHOD

### 2.1 The Plant

The Anacardium occidentale (Cashew) tree is easily cultivated in Malaysia predominantly alongside coastal areas. The leaves for this study were obtained from a cashew tree located near block N18 in Universiti Teknologi Malaysia (UTM).

### 2.2 Raw Extract Preparation

The cashew leaves were cleaned and left to dry for 3 to 5 days. The dried leaves were then pulverized to powder form (50-70 mesh) and stored in a dry place prior to extraction. The crude extract was prepared by Soxhlet extraction using 95 % ethanol (250 mL) for 18 hours at 78-80 °C. After that, the extracts were kept for further use in a cold dry place.

# 2.3 Determination of Adsorption Efficiency

The adsorption efficiency of AC on dark-coloured compounds in the raw extracts were evaluated by determining the percentage decrease of the absorbance at 420 nm; the higher the adsorption percentage, the higher the amount of dark-coloured compounds being removed. At the same time, it also indicates how light the extract's colour has become. A graph of adsorption (%) versus contact time for different compositions of activated carbon was plotted.

### 2.4 Antioxidant Assay

The decolourized sample extracts were oven-dried after the decolourization treatment. The dried solids were then diluted in dimethyl sulfoxide (DMSO) into solutions of concentrations 1mg/mL and 10 mg/mL. After that, 5  $\mu L$  of these test sample extracts were mixed with 95  $\mu L$  of 1,1-Diphenyl-2-picrylhydrazyl, (DPPH, 300 M) in ethanol. The mixtures were incubated at 37 °C for 30 min, and then the absorbances were measured at 570 nm. From there, the Radical Scavenging Capacity (RSC), expressed as a percentage was calculated. Ascorbic acid was used as a standard [7], [12]. A graph of RSC percentage for extracts with 1mg/mL and 10 mg/mL concentration treated by different compositions of activated carbon versus contact time was plotted.

# 2.5 Determination of Optimum Contact Period and Activated Carbon Composition

The decolourization device was assembled as presented in Figure 1. The original absorbance of the sample extracts was measured at 420 nm before any treatments were carried out. With raw extracts of natural pH and at room temperature (25°C), 100 mL of raw extracts were inserted into the device layered with ACs (powdered AC layered above granular AC). The ratio of powdered AC to granular AC was manipulated to 0:1, 1:1, and 2:1, with the amount of granular AC maintained at 5 g in all

three. The amount of granular AC was not manipulated because a previous study has shown that there were no increment in adsorption efficiency of dark-coloured compounds even in higher amounts [1]. For each of different AC ratios, raw extracts were left in the device for contact periods of 10, 20, 30, 40, 50, and 60 minutes. After the treatments, the treated sample extracts were measured their absorbance at 420 nm. The optimum contact period and composition of AC for adsorption efficiency were determined from the results.

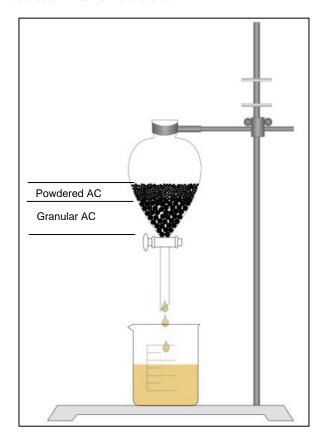


Figure 1 Diagram of herbal extract decolourization device

# 2.6 Quality Analysis

All treated raw extracts were dried and then dissolved into concentrations of 1 mg/mL and 10 mg/mL. The quality of the treated sample solutions was determined by antioxidant analysis. The optimum operating conditions for decolourization device were determined from the analysis.

# 2.7 Determination of Isothermal Model

Linearized graphs were plotted to determine the adsorption isotherm that best fits the designed decolourization device. The graph with model that best fits the system. All the calculations for each isotherm were based on the following equations [13].

Langmuir: 
$$\frac{A_e}{q_e} = \frac{1}{bQ^o} + \frac{A_e}{Q^o}$$
 (1)

Where

b (1/a.u.) is the Langmuir constant

Q° ((a.u.) m³ sample extract/kg AC) is the amount of adsorption corresponding to monolayer coverage.

Both b and  $Q^{\text{o}}$  were obtained from linearized plots of  $(A_{\text{e}}/q_{\text{e}})$  versus  $A_{\text{e}}.$ 

Freundlich: 
$$\ln q_e = \ln K_f + \frac{1}{n} \ln A_e$$
 (2)

Where

K<sub>f</sub> (a.u.) m<sup>3</sup> sample extract/kg AC 1/n is the Freundlich constants

Both  $K_{\rm f}$  and 1/n were obtained from linearized plots of ln  $q_{\rm e}$  versus  $ln A_{\rm e}.$ 

Frumkin: 
$$q_e = n_T ln K_T + n_T ln A_e$$
 (3)

Where  $n_T$  and  $K_T$  are the Frumkin constants.

Both  $n_T$  and  $K_T$  were obtained from linearized plots of  $q_e$  versus  $ln A_e. \label{eq:constraint}$ 

Where A and B are the Temkin constants.

Both A and B were obtained from linearized plots of  $q_{\rm e}$  versus (lnAe/qe).

# ■3.0 RESULT AND DISCUSSIONS

# 3.1 Optimum Contact Period and Activated Carbon Composition

From section 2.5, it was found that an AC ratio of 2:1 (10 g powdered AC, 5 g granular AC) and at a contact period of 10 min lead to the highest adsorption efficiency (99%). In fact, 10 min was always the most efficient contact period for all AC compositions as illustrated in Figure 2. Evidently, a longer contact period would unnecessarily prolong the process of obtaining similar results and may affect the extracts' quality [4]. For AC composition, it would appear that the lower the powdered AC content, the lower the adsorption efficiency. AC compositions of 1:1 (5 g powdered AC, 5 g granular AC) yielded an efficiency of 93% while the AC ratio of 0:1 (0 g powdered AC, 5 g granular AC) yielded 13% only. The decrease of adsorption efficiency is due to the decrease of the number of adsorption sites [1], [4].

The differences in colours of the treated samples are shown in Figure 3. To the naked eye, it would seem that the effects of AC composition on treated sample colours of 1:1 and 2:1 are similar while 0:1 is a lot darker than the other two. Together with a previous study that established that higher amounts of granular AC invoked no increment in adsorption efficiency of dark-coloured compounds [1], the results of the current study agrees with another study that powdered AC are more suitable for colour adsorption in terms of adsorption efficiency [14].

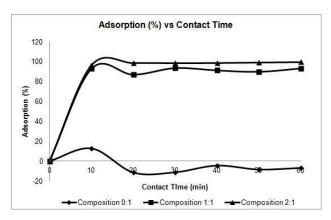


Figure 2 Graph Adsorption (%) versus Contact Time for different composition of activated carbon

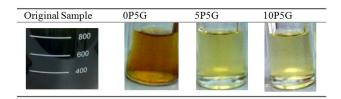
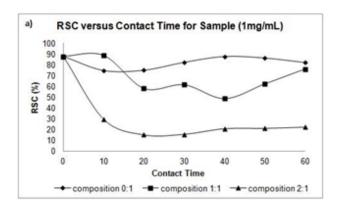


Figure 3 The colour of cashew leaves extract before and after 10 minutes contact time within the device

## 3.2 Quality of Treated Extract

The results (Figure 4a and 4b) suggest that antioxidant activity (the ability to scavenge free radicals) increases with sample concentration. Samples treated with the device with AC composition of 0:1 and 1:1 were able to retain 85-88% of their ability to scavenge free radicals. On the other hand, the device with AC composition of 2:1 reduced the sample's ability to scavenge free radicals to an average of 45% only. Due to the fact that the device with AC composition of 1:1 was able to very stably and efficiently reduce sample colour (93 %) while maintaining high antioxidant activity, it was chosen as the best AC composition for the device to adsorb dark-coloured compounds.



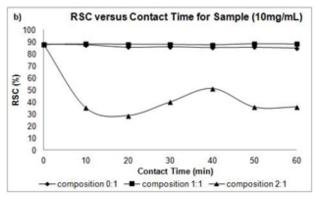


Figure 4 Graph RSC (%) for (a) 1mg/mL and (b) 10 mg/mL samples versus contact time for different composition of activated carbon

#### 3.3 Isotherms Model

The parameters of isotherm equations (Langmuir, Freundlich, Frumkin and Temkin) for the adsorption of dark-colour compounds on this decolourization system's AC, the sum of error squares (SSE) and R values were calculated by using linear regression analysis (Figure 5 and Table 1). The isotherm model that has the highest R value and the lowest SSE value is the model that best suits the experimental data (Table 2) [1]. Of the four isotherm models, the Langmuir isotherm (Figure 5a) is found to be the best fit for the experimental data since it has the highest R value (0.9996) and the lowest SEE value (2.616  $\times$  107).

The results indicates that the adsorption of dark-coloured compounds by the newly designed decolourization device is linear and irreversible at the composition and temperature (25°C) used [12], [13]. The Langmuir and Freundlich isotherm models have been listed in most of the previous studies as the adsorption models that is sufficient to describe the equilibrium adsorption data and determine the isotherm parameters for total phenolic content and dark-coloured compound adsorption [1, 2], [4, 5], [14, 15].

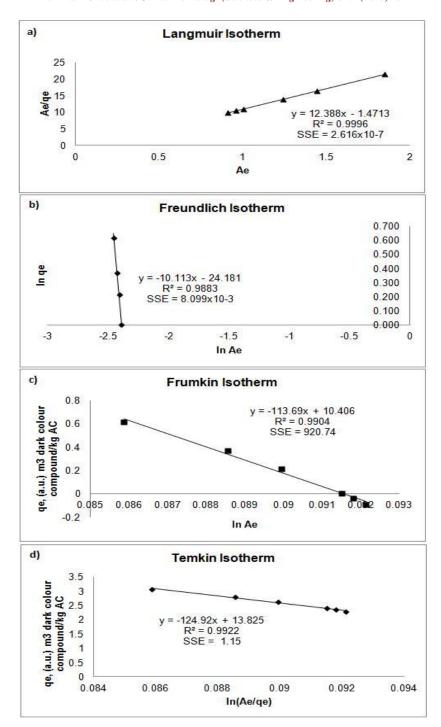


Figure 5 Graph of (a) Langmuir, (b) Freundlich, (c) Frumkin, (d) Temkin isotherm for dark colour compounds (linear regression analysis) on activated carbon at temperature  $25^{\circ}$ C

Table 1 Langmuir, Freundlich, and Temkin constants for sorption of dark colour compound at different temperatures using the linear regression analysis

Contact time (min)	10	20	30	40	50	60
$A_{o}$	14.730	14.730	14.730	14.730	14.730	14.730
$A_{\rm e}$	1.003	1.850	0.910	1.240	1.447	0.960
Q <sub>e exp</sub>	0.09151	0.08587	0.09213	0.08993	0.08855	0.09180
$A_e/q_e$	10.960	21.545	9.877	13.788	16.340	10.458
$ln(A_e/q_e)$	2.394	3.070	2.290	2.624	2.794	2.347
lnq <sub>e</sub>	-2.391	-2.455	-2.385	-2.409	-2.424	-2.388
lnA <sub>e</sub>	0.003	0.615	-0.094	0.215	0.369	-0.041

Table 2 Parameters in isotherm equation for the adsorption of dark colour compounds at 25°C with AC composition of 1:1

Isotherm Models	Adsorption Parameters	Temperature: 25°C	
Langmuir	Q°	0.08072	
	b	-8.420	
	R	0.9998	
	SSE	$2.616 \times 10^{-7}$	
Freundlich	$K_{\mathrm{f}}$	0	
	1/n	-10.113	
	R	0.9883	
	SSE	$8.099 \times 10^{-3}$	
Frumkin	$K_{\mathrm{T}}$	0.9125	
	$n_{\mathrm{T}}$	-113.69	
	R	0.9904	
	SSE	920.74	
Temkin	A	13.825	
	В	-124.92	
	R	0.9961	
	SSE	1.15	

### ■4.0 CONCLUSION

The decolourization device's optimum operating conditions for decolourizing 100 mL of cashew leaf extracts were found to be with an AC composition 1:1 (5 g of powdered AC, 5g of granular AC), at a temperature of 25°C for a contact period of 10 min. Such conditions reduced 81% total phenolic content and retained 88% radical scavenging capacity of cashew leaf extracts. The design of this system best fits Langmuir isotherm which demonstrates monolayer coverage of the phenolic and darkcoloured compounds at the outer surface of AC. Hence, the use AC is a good alternative for removing phenolic and dark-coloured compounds from cashew leaf extracts. Based on the data obtained, it was found that cashew leaf extract decolourization can be manipulated to suit the needs of end-users by controlling the contact period. This newly designed decolourization device should be very suitable for other herbal extracts as well as it can be optimized by simply adjusting the ratio of granular and powdered activated carbon.

# Acknowledgement

The author wishes to gratefully acknowledge the Institute of Bioproduct Development (IBD) and the Department of Bioprocess Engineering, Universiti Teknologi Malaysia (Johor Bahru) for the facilitating in the project.

# References

- [1] Arslanoğlu, F. N., F. Kar, and N. Arslan. 2005. Adsorption of Dark Coloured Compounds from Peach Pulp by Using Granular Activated Carbon. *Journal of Food Engineering*. 68(4): 409–417. DOI: 10.1016/j.jfoodeng.2004.06.017.
- [2] Soto, M. L., A. Moure, H. Domínguez, et al. 2008. Charcoal adsorption of Phenolic Compounds Present in Distilled Grape Pomace. *Journal of Food Engineering*. 84(1): 156–163. DOI: 10.1016/j.jfoodeng.2007.04.030.
- [3] Sessa, D. J., F. J. Eller, D. E. Palmquist, et al. 2003. Improved Methods for Decolourizing Corn Zein. Industrial Crops and Products. 18(1): 55– 65. DOI: 10.1016/s0926-6690(03)00033-5.
- [4] Carabasa, M., A. Ibarz, S. Garza, et al. 1998, Removal of Dark Compounds from Clarified Fruit Juices by Adsorption Processes. Journal of Food Engineering. 37(1): 25–41. DOI: 10.1016/S0260-8774(98)00075-2.
- [5] Richard, D., M. d. L. Delgado Núñez, and D. Schweich. 2009. Adsorption of Complex Phenolic Compounds on Active Charcoal: Adsorption Capacity and Isotherms. *Chemical Engineering Journal*. 148(1): 1–7.
- [6] Mukherjee, S., S. Kumar, A. K. Misra, et al. 2007. Removal of Phenols from Water Environment by Activated Carbon, Bagasse Ash and Wood Charcoal. Chemical Engineering Journal. 129(1–3): 133–142.
- [7] Abas, F., N. H. Lajis, D. A. Israf, et al. 2006. Antioxidant and Nitric Oxide Inhibition Activities of Selected Malay Traditional Vegetables. Food Chemistry. 95(4): 566–573. DOI: 10.1016/j.foodchem.2005.01.034.

- [8] Gaffar, R. A., N. E. S. Sazali and F. A. A. Majid. 2008. Colour Reduction And Anti-microbial Evaluation of Pre-treated Cashew Leaves Extract. *Journal of Chemical and Natural Resources Engineering*. 2(Special): 1–9
- [9] Abdul Gaffar, R., F. A. Abdul Majid, and M. R. Sarmidi. 2008. Tyrisonase Inhibition and Melanin Reduction of Human Melanocytes (Hemn-MP) Using Anacardium Occidentale L Extract. *The Medical Journal of Malaysia*. 63 Suppl A: 100–101.
- [10] Konan, N. A. and E. M. Bacchi. 2007. Antiulcerogenic Effect and Acute Toxicity of a Hydroethanolic Extract from the Cashew (Anacardium occidentale L.) leaves. *Journal of Ethnopharmacology*. 112(2): 237–242. DOI: 10.1016/j.jep.2007.03.003.
- [11] Odara Horta Boscolo, L. R. R. M. V. F., Luci de Senna Valle. 2010. An Ethnobotanical Survey as Subsidy for the Generation of Researches Related to Biotechnology. *International Research Journal of Biotechnology*. 1(1): 1–6.
- [12] Bozin, B., N. Mimica-Dukic, I. Samojlik, et al. 2008. Phenolics as Antioxidants in Garlic (Allium sativum L., Alliaceae). Food Chemistry. 111(4): 925–929. DOI: 10.1016/j.foodchem.2008.04.071.
- [13] Kadirvelu, K. and C. Namasivayam. 2003. Activated Carbon from Coconut Coirpith as Metal Adsorbent: Adsorption of Cd(II) from Aqueous Solution. Advances in Environmental Research. 7(2): 471–478. DOI: 10.1016/S1093-0191(02)00018-7.
- [14] Caqueret, V., S. Bostyn, B. Cagnon, et al. 2008. Purification of Sugar Beet Vinasse - Adsorption of Polyphenolic snd Dark Coloured Compounds on Different Commercial Activated Carbons. Bioresource Technology. 99(13): 5814–5821. DOI: 10.1016/j.biortech.2007.10.009.
- [15] Simaratanamongkol, A. and P. Thiravetyan. 2010. Decolourization of Melanoidin by Activated Carbon Obtained from Bagasse Bottom Ash. Journal of Food Engineering. 96(1): 14–17. DOI: 10.1016/j.jfoodeng.2009.06.033.