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# **Treatment of Food Processing Industrial Effluent** Using Coagulation and Sequential Batch Reactor

Azmi Aris, M.Eng Department of Environmental Engineering Faculty of Civil Engineering, UTM

> H. P. Siang, M.Sc K. K. Tan, B.Sc Tropical Interest Sdn. Bhd.

#### ABSTRACT

The performance of combined treatment processes, namely coagulation and Sequential Batch Reactor (SBR) to treat effluent from food processing industry was evaluated. The experimental study was conducted in a batch mode using pilot-scale reactor. The parameters used in assessing the treatment system were BOD<sub>5</sub>, COD and SS. The optimum amount of chemicals for the coagulation process ranges from 20 mg/L to 80 mg/L for coagulant and 60 mg/L to 220 mg/L for polymer while the optimum pH ranges from 5.5 to 7.0. The compliance of Standard A of the Environmental Quality Act was met using the combined process with SBR retention time of 6 hours.

## INTRODUCTION

Unlike domestic wastewater, the characteristics of industrial wastewater are rather complex and vary from time to time in term of flow and strength. As an industry may produce several products, each of the product manufacturing processes produces wastewater of different volume and composition. Only small number of industrial plants operate continuously that generate wastewater of non-varying characteristics while majority of industries do not operate 24 hours a day and do not attempt to produce either product or effluent continuously or consistently [1]. Due to these variations and also to the complexity of chemicals that are used in the manufacturing processes, in many cases, more than one treatment process is needed in order to treat the wastewater to the acceptable quality.

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In this study, the feasibility of treating effluent from a food manufacturing industry was evaluated. The industry consists of several manufacturing plants which include beverage, poultry processing, canned food, snack food, and sauce plants. The generated wastewater contains colloidal solids, colouring compounds, suspended solids, oil, and grease. As many alternatives are available, the study focus on the possibility of using coagulation and conventional SBR to treat the wastewater. The objective is to remove the organics and suspended solids (SS) from the wastewater so as to comply with either Standard A or Standard B (Table 1) as stipulated by the Department of Environment (DOE), Malaysia [2]. The parameters of concern in the study include COD,  $BOD_{5}$ , and SS.

Parameters	Standard A (mg/L)	Standard B (mg/L)
COD	50	100
BOD <sub>5</sub>	20	50
SS	50	100

 Table 1 DOE standards with respect to the evaluated parameters.

#### MATERIALS AND METHODS

Samples for the study were taken from a nearby food manufacturing industry while the coagulant and polymer were obtained from a chemical supplier. Chemicals that were used for analytical work were of reagent grade and the analytical work were conducted based on the standard procedures [2].

The study was conducted in two stages. The first stage was to determine the optimum amount of chemicals and pH to be used in the coagulation process while the second was to determine the effectiveness of the whole treatment system (coagulation + SBR) by varying the SBR hydraulic retention time (HRT).

Optimisation of the chemicals and pH for the coagulation process was conducted using typical jar test procedures. The dose of coagulant and polymer tested ranged from 20 mg/L to 220 mg/L, each, while the pH tested ranged from 5.5 to 8.5. Study on the SBR was conducted using a pilot scale reactor. The reactor is 1 m high with a diameter of 0.4 m and total filled volume of 85 L. The microorganisms in the SBR were acclimatised for about one and half month within which the mixed liquor suspended solids (MLSS) reached about 3000 mg/L. Throughout the study, MLSS and dissolved oxygen (DO) content in the SBR were maintained not to be less than 3000 mg/L and 3 mg/L, respectively. Once the SBR was ready, the whole treatment system was put into test. The raw wastewater was pretreated with coagulation process using a pilot mixer (40 L) and was then fed into the SBR with a filling time of about 2 hours. The performance of the system was studied for different SBR retention times (i.e. 15, 30, 60, 120, 240, 360 and 480 minutes) with settling time of 2 hours. At least two trials were conducted for each retention time in order to get representative results.

## **RESULTS AND DISCUSSIONS**

The characterisics of the raw wastewater during the study period is given in Table 2. The wastewater can be characterised as containing high organic content, colloidal in nature and acidic.

Parameter	Concentration Range
pH	4 – 5.5
Biochemical Oxygen Demand (BOD <sub>5</sub> )	200 – 2500 mg/L
Chemical Oxygen Demand (COD)	600 – 6000 mg/L
Suspended Solids (SS)	50 – 1300 mg/L

Table 2 Raw wastewater characteristics obtained during the study period.

#### **Separation Process**

Results for jar test study are given in Tables 3 to 5. Based on percentage of COD removed, with the variation of raw wastewater quality, the optimum amount of coagulant ranged from 20 mg/L to 80 mg/L. The optimum pH ranged from 5.5 to 7.0 while the optimum amount of polymer ranged from 60 mg/L to 220 mg/L. On average, the highest percentage of removal was achieved using coagulant dose of 80 mg/L, pH 6.5, and polymer dose of 180 mg/L. During the jar test study, average percentage of COD removal varied from 72% to 82% following the addition of chemicals and pH adjustment.

Although highest average percentage of removal was obtained using polymer dose of 180 mg/L, acceptable amount of COD removal ( $\geq$  70%) occurred throughout the polymer doses. Thus, for economic reason, lower coagulant and polymer doses (than the optimum ones) could be used in the actual treatment process. During the second stage study, the pretreatment of raw wastewater prior to SBR was carried out using 80 mg/L dose of coagulant and polymer, each, at pH 7.

	Initial		mg/L coagulant									
Run #	Initial COD (mg/L)	2 0	4 0	6 0	8 0	1 0 0	1 2 0	1 4 0	1 6 0	1 8 0	2 0 0	2 2 0
					Per	centa	ge of F	temov	al			
1	854	5 3	6 7	7 3	8	2 5	5 1	4 4	2 3	8 6	3 0	5 2
2	3380	5 3	4 8	5 4	5 9	4 5	4 6	3 0	5 4	5 9	4 5	5 6
3	2685	8	8 0	7 8	6 8	7 8	5 0	8 4	7 9	7 1	8 6	7 8
4	1020	6 4	6 5	7 0	7 4	6 8	7 1	6 1	5 3	6 7	6 1	6 2
5	1870	6 7	7	4 9	6 4	5 8	5 5	5 4	5 8	6 4	4 9	5 3
Ave	rage	6 5	6 6	6 5	7 <b></b> 10 <b></b>	5 5	5 5	5 5	5 3	6 9	5 4	6 0

 Table 3 Percentage of COD removal following coagulant addition.



Highest removal percentage obtained in a run trial

 
 Table 4 Percentage of COD removal following coagulant addition and pH adjustment.

	Initial	рН								
Run	COD	5.5	6	6.5	7	7.5	8	8.5		
#	(mg/L)		I	Percenta	ge of R	emoval	• -			
1	3380	72	65	69	65	67	70	63		
2	2515	-	67	<b>1</b> 69	66	64	67	-		
3	2685	70	64	63	571	66	67	65		
4	1730	61	67	64	54	59	55	55		
5	1020	65	87	<b>1</b> 89	80	70	81	58		
6	1870	64	61	81	82	60	73	76		
Ave	rage	66	69	73	70	64	69	65		



Highest removal percentage obtained in a run trial

	Initial		mg/L polymer									
Run #	COD (mg/L)	2 0	4 0	6 0	8 0	1 0 0	1 2 0	1 4 0	1 6 0	1 8 0	2 0 0	2 2 0
					Pe	rcenta	ge of I	Remov	al			
1	854	7 5	7 5	9 2	8 3	7 9	8 7	8 3	8 4	9 1	8 0	8 4
2	3380	6 4	7 3	7 4	7 4	6 5	7 2	-	7 4	6 5	7 2	7 1
3	2515	6 8	6 8	5 1	6 0	5 2	6 0	6 1	6 3	-	7	6 4
4	2685	6 5	6 5	5 8	6 7	7 0	6 8	6 7	6 8	6 6	6 8	7. 1
5	1730	6 9	6 8	8	7 6	8 1	7	7 9	8 4	8 5	6 8	7 0
6	1020	-	8 6	8 3	8 1	8 0	7 5	9 3	8 7	8 7	8 3	9. 4
7	1870	9 3	9 3	8 6	9 3	9 4	9 5	9 5	9 16	9 5	9 4	9 5
Av	erage	7 2	7 5	7 6	7 6	7	7 6	8 0	7 9	8 2	7 7	7 8

Table 5 Percentage of COD removal following coagulant addition, pH adjustment and polymer addition.



Highest removal percentage obtained in a run trial

Although highest average percentage of removal was obtained using polymer dose of 180 mg/L, acceptable amount of COD removal (≥ 70%) occurred throughout the polymer doses. Thus, for economic reason, lower coagulant and polymer doses (than the optimum ones) could be used in the actual treatment process. During the second stage study, the pretreatment of raw wastewater prior to SBR was carried out using 80 mg/L dose of coagulant and polymer, each, at pH 7.

#### **SBR Process**

As reported in previous studies [4], the SBR has been used to treat a variety of wastewater either in combination with other processes or as a single treatment process. A summary of several SBR studies is given in Table 6. In general, better-than-90% organic removal efficiencies are reported.

Type of Wastewater	pe of Wastewater Influent (mg/L) (hour)		BOD Removal (%)
<ol> <li>Dairy</li> <li>Settled sewage</li> </ol>	2000 <sup>3</sup>	8/10/6(S+D)/0	90
	140	2.9/0.7/0.7/0.7/1.0	95
<ol> <li>Landfill leachate</li> <li>Hazardous wastes</li> <li>Baur causas</li> </ol>	$2300^4$	10/12/1/0.5/0.5	89
	1440 <sup>4</sup>	10/10/2/2(D+I)	81
	268	17.2(F+R)/0.83/0.37/0	98
<ol> <li>Raw sewage</li> <li>Raw piggery</li> <li>Anaerobically</li> </ol>	1075	3/16/1/0.5/3.5	98
	269	3/16/1/0.5/3.5	83
<ol> <li>Anacrobically</li></ol>	1200 <sup>3</sup>	4/6/6/1/0	92
pretreated piggery <li>Oleochemical</li> <li>Palm oil refinery</li>	1800	3/17.5/3/0.5/0	94

Table 6 Summary of SBR performance studies<sup>1</sup>.

<sup>1</sup> Adapted from [4]

<sup>2</sup>F = FILL; R = REACT; S = SETTLE; D = DECANT; I = IDLE

<sup>3</sup> based on COD

<sup>4</sup> based on TOC

Results for the SBR treated wastewater in this study are given in Tables 7 to 9 and is illustrated in Figure 1. As shown in Table 7, depending on the initial COD concentration, the treated COD ranged from 708 mg/L (HRT = 15 min) to 15 mg/L (HRT = 6 hours). During the study, the SBR treated wastewater almost complied with Standard B at HRT of 4 hours. At 6-hour retention time, the treated wastewater complied with Standard A with average COD of 15 mg/L (average of five trials). Percentage removal of the system ranges from from 73.8% at HRT of 15 minutes to 99.2% at HRT of 8 hours. Significant increase in COD removal could be observed at HRT of 4 hours.

As shown in Table 8, the BOD<sub>5</sub> of the treated wastewater ranges from 675 mg/L to less than 10 mg/L. Compliance of Standard B was observed at 2-hour HRT. However, possibly due to the contents of the wastewater, further reduction of BOD<sub>5</sub> could not be achieved until 4-hour HRT. At 4-hour HRT, BOD<sub>5</sub> was reduced to 20 mg/L and thus, complied with the Standard A. Increasing the HRT further reduced the BOD<sub>5</sub> to less than 10 mg/L. Percentage removal of BOD<sub>5</sub> ranges from 63.7% to 99.1%. Similar to COD, significant BOD<sub>5</sub> reduction was observed when the HRT was extended to 4 hours. Removal percentage of greater than 97% was observed at HRT of 4 hours and greater.

SBR HRT	Aver: (r	%	
(min)	Raw	SBR treated	Removal
15	2700	708	73.8
30	3000	228	92.4
60	1612	311	80.7
120	2623	291	88.9
240	4835	103	97.9
360	926	15	98.4
480	3603	30	99.2

Table 7 Removal of COD following coagulation and SBR treatment.

Table 8 Removal of BOD<sub>5</sub> following coagulation and SBR treatment.

SBR HRT	Avera (r	%	
(min)	Raw	SBR treated	Removal
15	1860	675	63.7
30	2540	87	96.6
120	700	175	75.0
240	2160	20	99.1
360	330	< 10	> 97.0
480	666	11	98.3

Results for SS are shown in Table 9. With raw SS value ranges from 183 mg/L to 1350 mg/L, the treated water complies with Standard A even at 15-minute retention time. Thus, SS is not considered as a limiting factor in the design of the treatment system. Although chemically treated wastewater was not analysed for SS, from its appearance, removal of SS could be achieved by using the coagulation process.

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#### CONCLUSION

The feasibility of treating food manufacturing industrial effluent using coagulation and SBR to the standard set by the DOE was evaluated in the study. With respect to the considered parameters (i.e. BOD<sub>5</sub>, COD, and SS), the combination processes were found to be adequate in fulfilling the requirements.

For coagulation, the optimum chemicals concentration ranges from 20 to 80 mg/L and from 60 mg/L to 220 mg/L for coagulant and polymer, respectively. The optimum pH ranges from 5.5 to 7.5. With respect to the tested parameters, compliance with Standard B was achieved at SBR HRT of 4 hour while full compliance with Standard A was achieved at SBR HRT of 6 hours.

SBR HRT	Ave (1	%	
(min)	Raw	SBR treated	Removal
15	720	20	97.2
30	892	45	95.0
60	443	26	94.1
120	1350	23	98.3
240	-	17	-
480	183	12	93.4

Table 9 Removal of SS following coagulation and SBR treatment.

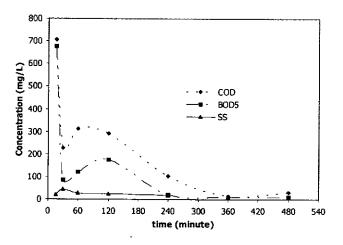


Figure 1 Profile of SBR treated wastewater.

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